

# A FUNDAMENTAL EQUATION FOR DESCRIBING THE RELATIONSHIP BETWEEN THE COMPOSITION OF THE MULTICOMPONENT MOBILE PHASE AND CHROMATOGRAPHIC RETENTION

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## ABSTRACT

A fundamental equation for describing the relationship between the composition of the multicomponent mobile phase (CMCMP) and chromatographic retention (CRV)

$$\ln k' = a + \sum_{i=1}^n b_i c_{B_i} + \sum_{i=1}^n c_i \ln c_{B_i},$$

is derived by using statistical thermodynamic method. The equation is proven by a ternary mobile phase experiment for 11 compounds. Based on this equation, we also obtain retention equations for weak dissociative solute.

## I. INTRODUCTION

In liquid-solid chromatography (LSC), to derive a good relationship between the composition of the mobile phase and the retention value is still an interesting subject. Many researches on it have been made for binary mobile phase<sup>[1-5]</sup>. Recently, there is an emphasis on the use of multicomponent mobile phase for satisfactory separation<sup>[6]</sup>. Therefore, great attention is paid to the research on the relationship between the composition of the multicomponent mobile phase and retention value. Snyder reported the relationship between the composition of the mobile phase and solvent strength<sup>[7-8]</sup> so that it can predict the retention value of sample from the solvent strength. For binary solvent, Snyder's equation is:

$$\varepsilon_{ab} = \varepsilon_a + \frac{\log(N_b 10^{\alpha' n_b (\varepsilon_a - \varepsilon_b)} + 1 - N_b)}{\alpha' n_b}. \quad (1)$$

Eq. (1) can be rewritten as<sup>[8]</sup>

$$\varepsilon_{ab} = \varepsilon_a + \frac{\log(N_a / \theta_a)}{\alpha' n_b}. \quad (2)$$

In Eq. (1) and Eq. (2),  $\varepsilon_a$  and  $\varepsilon_b$  are solvent strength values ( $\varepsilon^0$ ) for solvents A and B,  $n_b$  is the cross-sectional area of a molecule of B,  $N_a$  and  $N_b$  refer to the mole fractions in mobile phase for solvents A and B respectively, and  $\theta_a$  is the mole fraction of A in the stationary phase. A similar equation was presented by

Snyder and Glajch for multicomponent mobile phase.

These equations can be used only for less polar solvents B but can not be used for more polar B solvents because of localization effect. Snyder and Glajch considered the effect of localization on the calculation of the solvent strength. They gave an expression to calculate the localization function as an approximation for calculating  $\epsilon^0$  value. However, it is only an empirical expression.

Based on the solubility parameter theory, Schoenmakers presented an equation for describing the relationship between the composition of the ternary mobile phase and the capacity factor of sample in reversed phase liquid chromatography (RPLC)<sup>[9]</sup>

$$\ln k'_i = A_1\varphi_1^2 + A_2\varphi_2^2 + B_1\varphi_1 + B_2\varphi_2 + C + D\varphi_1\varphi_2, \quad (3)$$

where,  $\varphi_1$  and  $\varphi_2$  refer to the volume fractions of two organic modifiers in mobile phase respectively,  $k'_i$  is the capacity factor of solute  $i$ ,  $A_1, A_2, B_1, B_2, C$  and  $D$  all are constants which relate to sample and stationary phase. Eq. (3) gives a more accurate description of variation of retention with composition in certain concentration range in ternary RPLC system. However, when mobile phases of high water content ( $\varphi_1 + \varphi_2 \leq 0.1$ ) are used, Eq. (3) is insufficient<sup>[9,10]</sup>, it can only be used in a limited concentration range.

In this paper, we theoretically derive a fundamental equation for describing the relationship between the composition of the multicomponent mobile phase and sample capacity factor by using statistical thermodynamic method<sup>[11]</sup>. Our experimental results prove that the fundamental equation can predict the retention value accurately in wide concentration range. In addition, retention equations are given for weak dissociative solute by using the equilibrium principle of weak dissociative solute and chemical dynamic method.

## II. THE DERIVATION OF CHROMATOGRAPHIC RETENTION EQUATION FOR NON-DISSOCIATIVE SOLUTION SYSTEM

Consider an isolated system which has no material exchange with outside circumstance. The system contains the solute A, solvents  $B_1, B_2, \dots, B_n$  and adsorbent S

In the system, the total partition function  $Q$  is

$$Q = (T_A \cdot J_A)^{N_A} \cdot \prod_{i=1}^n (T_{B_i} \cdot J_{B_i})^{N_{B_i}} \cdot \mathcal{Q}, \quad (4)$$

where  $T_A, T_{B_i}$  are the translational partition functions of the solute A and solvent  $B_i$ ,  $J_A, J_{B_i}$  are the internal partition functions respectively. As

$$N_A \ll N_{B_1}, N_{B_2}, \dots, N_{B_n},$$

the interaction between solute molecule A as well as between molecule A and solvent molecules  $B_i$  can be neglected. The configuration partition function,  $\mathcal{Q}$ , can be expressed as:

$$Q = \frac{1}{N_A! \prod_{i=1}^n N_{B_i}!} \int \dots \int e^{-\frac{1}{kT} [\chi_A N_A + \sum_{i=1}^n (\chi_{B_i} N_{B_i})]} \cdot (d\omega_A)^{N_A} \cdot \prod_{i=1}^n (d\omega_{B_i})^{N_{B_i}}, \quad (5)$$

where  $\chi$  refers to the potential of the molecule in the solution. According to the smoothed potential model, we can obtain:

$$Q = \frac{1}{N_A! \prod_{i=1}^n N_{B_i}!} e^{-\frac{1}{kT} [\chi_A N_A + \sum_{i=1}^n (\chi_{B_i} N_{B_i})]} \cdot V_0^{(N_A + \sum_{i=1}^n N_{B_i})}, \quad (6)$$

where  $V_0 = N_A V_A + \sum_{i=1}^n N_{B_i} V_{B_i}$  is the total volume of solution in the system and  $V_A, V_{B_i}$  are the volumes of individual molecule in the liquid phase.

The Helmholtz function of solution is:

$$\begin{aligned} F &= -RT \ln Q \\ &= -RT \left\{ -\ln N_A! - \sum_{i=1}^n \ln N_{B_i}! - \frac{1}{kT} \left[ \chi_A N_A + \sum_{i=1}^n (\chi_{B_i} N_{B_i}) \right] \right. \\ &\quad \left. + \left( N_A + \sum_{i=1}^n N_{B_i} \right) \ln V_0 + N_A \ln (J_A \cdot T_A) + \sum_{i=1}^n [N_{B_i} \ln (T_{B_i} J_{B_i})] \right\}. \end{aligned} \quad (7)$$

Therefore, the chemical potential of solute A in the solution is:

$$\begin{aligned} \mu_A = \frac{\partial F}{\partial N_A} \Big|_{T,V} &= -RT \left\{ -\ln N_A - \sum_{i=1}^n \frac{\partial N_{B_i}}{\partial N_A} \ln N_{B_i} - \frac{1}{kT} \left( \chi_A + \sum_{i=1}^n \chi_{B_i} \frac{\partial N_{B_i}}{\partial N_A} \right) \right. \\ &\quad \left. + \left( 1 + \sum_{i=1}^n \frac{\partial N_{B_i}}{\partial N_A} \right) \ln V_0 + \ln (J_A \cdot T_A) + \sum_{i=1}^n \left[ \frac{\partial N_{B_i}}{\partial N_A} \ln (T_{B_i} \cdot J_{B_i}) \right] \right\}. \end{aligned} \quad (8)$$

The numbers of adsorbed molecules A,  $B_1, \dots, B_n$  which have potential  $\chi_A^a, \chi_{B_1}^a, \dots, \chi_{B_n}^a$  denote  $N_A^a, N_{B_1}^a, \dots, N_{B_n}^a$ . According to the ideal localized monolayers model, the partition function of the adsorbent surface is:

$$Q^a = \frac{N_s}{N_A^a! \prod_{i=1}^n N_{B_i}^a!} e^{-\frac{1}{kT} [\chi_A^a N_A^a + \sum_{i=1}^n (\chi_{B_i}^a N_{B_i}^a)]} \cdot (J_A^a)^{N_A^a} \cdot \prod_{i=1}^n (J_{B_i}^a)^{N_{B_i}^a}, \quad (9)$$

where  $N_s = N_A^a + \sum_{i=1}^n N_{B_i}^a$  refers to the number of the adsorbed molecule on the adsorbent surface. The Helmholtz function of adsorbent surface can be written as follows:

$$\begin{aligned} F^a &= -RT \ln Q^a \\ &= -RT \left\{ \ln N_s! - \ln N_A^a! - \sum_{i=1}^n \ln N_{B_i}^a! - \frac{1}{kT} \left[ \chi_A^a N_A^a + \sum_{i=1}^n (\chi_{B_i}^a N_{B_i}^a) \right] \right\} \end{aligned}$$

$$+ N_A^a \ln J_A^a + \sum_{i=1}^n N_{B_i}^a \ln J_{B_i}^a. \quad (10)$$

The chemical potential of solute A on the adsorbent surface therefore can be obtained

$$\begin{aligned} \mu_A^a = -RT \left\{ \left( 1 + \sum_{i=1}^n \frac{\partial N_{B_i}^a}{\partial N_A^a} \right) \ln N_s - \ln N_A^a - \sum_{i=1}^n \left( \frac{\partial N_{B_i}^a}{\partial N_A^a} \ln N_{B_i}^a \right) \right. \\ \left. - \frac{1}{kT} \left[ \chi_A^a + \sum_{i=1}^n \left( \frac{\partial N_{B_i}^a}{\partial N_A^a} \chi_{B_i}^a \right) \right] + \ln J_A^a + \sum_{i=1}^n \left( \frac{\partial N_{B_i}^a}{\partial N_A^a} \ln J_{B_i}^a \right) \right\}. \quad (11) \end{aligned}$$

Because of isolated system, it has no material exchange with outside circumstance, therefore

$$\partial N_A^a = -\partial N_A, \quad (12)$$

$$\partial N_{B_i}^a = -\partial N_{B_i}, \quad (13)$$

then

$$\frac{\partial N_{B_i}^a}{\partial N_A^a} = \frac{\partial N_{B_i}}{\partial N_A}. \quad (14)$$

Substituting Eq. (14) into Eq. (11), we obtain

$$\begin{aligned} \mu_A^a = -RT \left\{ \left( 1 + \sum_{i=1}^n \frac{\partial N_{B_i}}{\partial N_A} \right) \ln N_s - \ln N_A^a - \sum_{i=1}^n \left( \frac{\partial N_{B_i}}{\partial N_A} \ln N_{B_i}^a \right) \right. \\ \left. - \frac{1}{kT} \left[ \chi_A^a + \sum_{i=1}^n \left( \frac{\partial N_{B_i}}{\partial N_A} \chi_{B_i}^a \right) \right] + \ln J_A^a + \sum_{i=1}^n \left( \frac{\partial N_{B_i}}{\partial N_A} \ln J_{B_i}^a \right) \right\}. \quad (15) \end{aligned}$$

Both chemical potentials of solute A in the solution and on the adsorbent surface are equal at equilibrium. We obtain

$$\begin{aligned} \ln k' = \ln \frac{N_A^a}{N_A} = \sum_{i=1}^n \left( \frac{\partial N_{B_i}}{\partial N_A} \ln \frac{N_{B_i}}{N_{B_i}^a} \right) + \left( 1 + \sum_{i=1}^n \frac{\partial N_{B_i}}{\partial N_A} \right) \ln \frac{N_s}{V_0} + \ln \left( \frac{J_A^a}{T_A \cdot J_A} \right) \\ + \sum_{i=1}^n \left[ \frac{\partial N_{B_i}}{\partial N_A} \ln \left( \frac{J_{B_i}^a}{T_{B_i} J_{B_i}} \right) \right] + \frac{1}{kT} \left\{ \chi_A - \chi_A^a + \sum_{i=1}^n \left[ \frac{\partial N_{B_i}}{\partial N_A} (\chi_{B_i} - \chi_{B_i}^a) \right] \right\}. \quad (16) \end{aligned}$$

The potential of molecule A in the solution,  $\chi_A$ , includes the Van der Waals interaction energy and hydrogen bond energy involved the molecule A, therefore, the  $\chi_A$  can be written as

$$\chi_A = \sum_{i=1}^n Z_{AB_i} E_{AB_i} + E_{AH}, \quad (17)$$

where  $E_{AH}$  is the hydrogen bond energy of molecule A,  $E_{AB_i}$  refers to the Van der Waals energy of the each pair of adjacent molecules A- $B_i$ ,  $Z_{AB_i}$  is the number of molecule B, surrounding molecule A.

If we think the meeting each other of the molecules as a random process, the number of molecule  $B_i$  surrounding molecule A is proportional to the concentration

of solvent  $B_i$  in the solution, that is

$$Z_{AB_i} = K_{AB_i} \cdot c_{B_i}, \quad (18)$$

where  $K_{AB_i}$  is a constant relating to molecule size.

Substituting Eq. (18) into Eq. (17), we obtain

$$\chi_A = \sum_{i=1}^n K_{AB_i} E_{AB_i} c_{B_i} + E_{AH}. \quad (19)$$

In the same way, we can write the potential energy of an adsorbed molecule A as follows:

$$\chi_A^a = \sum_{i=1}^n K_{AB_i}^a E_{AB_i} c_{B_i} + E_A^a, \quad (20)$$

where  $E_A^a$  is the adsorption energy of molecule A (If there is hydrogen bond between the adsorbed molecule A and solvent molecule, the term  $E_A^a$  also includes the hydrogen bond energy).

Therefore,

$$\chi_A - \chi_A^a = \sum_{i=1}^n (K_{AB_i} - K_{AB_i}^a) E_{AB_i} c_{B_i} + E_{AH} - E_A^a \quad (21)$$

and

$$\chi_{B_i} - \chi_{B_i}^a = \sum_{j=1}^n (K_{B_i B_j} - K_{B_i B_j}^a) E_{B_i B_j} c_{B_j} + E_{B_i H} - E_{B_i}^a. \quad (22)$$

We used Langmuir adsorption isotherm for multicomponent adsorption and obtained an equation for describing the relationship between the composition and retention<sup>[12]</sup>

$$\ln k' = a' + b' \ln \left( 1 + \sum_{i=1}^n k_i c_{B_i} \right) + \sum_{i=1}^n c'_i c_{B_i} \quad (23)$$

where  $a'$ ,  $b'$ ,  $k_i$  and  $c'_i$  are constants.

Eq. (23) was proven by Dai Chaozheng and Chen Bailin with a ternary mobile phase experiment<sup>[13]</sup>. However, it is difficult to obtain the constants in the Eq. (23) from experimental data. On the other hand, under the liquid chromatography condition, Freundlich isotherm is better than Langmuir's for multicomponent adsorption, by using Freundlich isotherm,

$$N_{B_i}^a = N_s k_i c_{B_i}^{1/n_i}, \quad (24)$$

where  $k_i$  and  $n_i$  are constants and

$$c_{B_i} = \frac{V_{B_i}}{V_0} N_{B_i}. \quad (25)$$

We obtain

$$\frac{N_{B_i}^a}{N_{B_i}} = N_s k_i c_{B_i}^{\frac{1}{n_i} - 1} \cdot \frac{V_{B_i}}{V_0}. \quad (26)$$

Substituting Eqs. (21), (22), (26) into Eq. (16), the fundamental equation of retention of non-dissociative solute in the multicomponent mobile phase system of LSC can be derived as

$$\begin{aligned}
 \ln k' &= \ln \frac{N_s}{V_s} + \ln \frac{V_s}{V_0} + \sum_{i=1}^n \left[ \frac{\partial N_{B_i}}{\partial N_A} \ln \left( \frac{J_{B_i}^A}{T_{B_i} J_{B_i} k_i V_{B_i}} \right) \right] + \ln \left( \frac{J_A^A}{T_A J_A} \right) \\
 &+ \frac{1}{kT} \left[ E_{AH} - E_A^A + \sum_{i=1}^n \frac{\partial N_{B_i}}{\partial N_A} (E_{B_iH} - E_{B_i}^A) \right] \\
 &+ \sum_{i=1}^n \left[ \frac{\partial N_{B_i}}{\partial N_A} \left( 1 - \frac{1}{n_i} \right) \ln c_{B_i} \right] \\
 &+ \frac{1}{kT} \sum_{i=1}^n \left\{ (K_{AB_i} - K_{\Lambda B_i}^A) E_{AB_i} + \sum_{j=1}^n \left[ \frac{\partial N_{B_j}}{\partial N_A} (K_{B_j B_i} - K_{B_j B_i}^A) E_{B_j B_i} \right] \right\} c_{B_i} \\
 &= a + \sum_{i=1}^n c_i \ln c_{B_i} + \sum_{i=1}^n b_i c_{B_i}, \tag{27}
 \end{aligned}$$

where  $V_s$  is the volume of the absorbent,

$$\begin{aligned}
 a &= \ln \frac{N_s}{V_s} + \ln \frac{V_s}{V_0} + \sum_{i=1}^n \left[ \frac{\partial N_{B_i}}{\partial N_A} \ln \left( \frac{J_{B_i}^A}{T_{B_i} J_{B_i} k_i V_{B_i}} \right) \right] + \ln \left( \frac{J_A^A}{T_A J_A} \right) \\
 &+ \frac{1}{kT} \left[ E_{AH} - E_A^A + \sum_{i=1}^n \frac{\partial N_{B_i}}{\partial N_A} (E_{B_iH} - E_{B_i}^A) \right], \tag{27-1}
 \end{aligned}$$

$$b_i = \frac{1}{kT} \left\{ (K_{AB_i} - K_{\Lambda B_i}^A) E_{AB_i} + \sum_{j=1}^n \left[ \frac{\partial N_{B_j}}{\partial N_A} (K_{B_j B_i} - K_{B_j B_i}^A) E_{B_j B_i} \right] \right\}, \tag{27-2}$$

$$c_i = \frac{\partial N_{B_i}}{\partial N_A} \left( 1 - \frac{1}{n_i} \right). \tag{27-3}$$

It should point out that in the Eq. (27),  $\ln c_{B_i} \rightarrow -\infty$  when  $c_{B_i} \rightarrow 0$ , but when  $c_{B_i} = 0$ , the constant  $c_i = \frac{\partial N_{B_i}}{\partial N_A} \left( 1 - \frac{1}{n_i} \right)$  must be zero because  $N_{B_i} = 0$ . So the term  $c_i \ln c_{B_i} = 0$  when  $c_{B_i} \rightarrow 0$ . It is easy to find constants  $a$ ,  $b_i$ , and  $c_i$  from experimental data.

We prove Eq. (27) by using ternary mobile phase (hexane, ether and dichloromethane) for 11 solutes. In the experiment, the high performance liquid chromatograph LC-Series 4 (made in PERKIN-ELMER Company in U. S) is used, chromatographic column packed with  $5\mu$  silica is installed. Data processing is carried out on the Data Station 3600.

For ternary mobile phase, the Eq. (27) can be written as

$$\ln k' = a + b_1 c_{B_1} + b_2 c_{B_2} + c_1 \ln c_{B_1} + c_2 \ln c_{B_2}. \tag{28}$$

In the Table 1, the  $k'$  values calculated from Eq. (28) and those from the experiment are listed. There is a better coincide with both  $k'$  values in the wide concentration range. In the Table 2, we give the constants  $a$ ,  $b_1$ ,  $b_2$ ,  $c_1$  and  $c_2$

Table 1

The Experimental  $k'$  and Calculated  $k'$  for 4 Solutes at 35 Concentration Points of Ternary Mobile Phase

Concentration		Anthracene		Benzonitrile		Nitrobenzene		Benzyl Alcohol	
$c_{B_1}$	$c_{B_2}$	$k'_e$	$k'_c$	$k'_e$	$k'_c$	$k'_e$	$k'_c$	$k'_e$	$k'_c$
0.002	0.01	0.66	0.60	13.45	11.65	4.05	3.18	19.35	16.38
0.002	0.05	0.46	0.51	8.68	7.83	2.55	2.32	13.11	11.89
0.002	0.1	0.36	0.40	6.64	6.07	2.00	1.81	10.17	9.71
0.002	0.2	0.22	0.25	3.15	4.14	1.16	1.20	5.52	7.21
0.002	0.3	0.13	0.15	2.26	2.98	0.83	0.82	4.04	5.58
0.002	0.7	0.04	0.02	0.84	0.93	0.32	0.19	1.74	2.26
0.004	0.01	0.48	0.47	8.71	7.65	2.64	2.40	12.65	10.43
0.004	0.05	0.36	0.40	5.74	5.14	1.79	1.75	9.12	7.57
0.004	0.1	0.29	0.31	4.51	3.98	1.41	1.36	7.29	6.18
0.004	0.2	0.19	0.19	2.85	2.72	0.91	0.90	4.59	4.59
0.004	0.3	0.13	0.12	1.76	1.96	0.68	0.62	3.52	3.55
0.004	0.7	0.01	0.02	0.59	0.61	0.04	0.14	1.44	1.44
0.01	0.01	0.34	0.34	4.37	4.37	1.60	1.65	6.16	5.73
0.01	0.05	0.26	0.29	3.23	2.94	1.14	1.21	4.92	4.16
0.01	0.1	0.20	0.23	2.20	2.28	0.84	0.94	3.53	3.40
0.01	0.2	0.15	0.14	1.55	1.56	0.59	0.62	2.43	2.52
0.01	0.3	0.10	0.09	1.14	1.12	0.44	0.42	1.98	1.95
0.01	0.7	0.01	0.01	0.40	0.35	0.15	0.10	0.80	0.79
0.1	0.01	0.16	0.15	0.89	1.02	0.59	0.61	0.95	1.22
0.1	0.05	0.14	0.13	0.70	0.69	0.48	0.45	0.82	0.89
0.1	0.1	0.09	0.10	0.49	0.53	0.30	0.35	0.66	0.72
0.1	0.2	0.06	0.06	0.34	0.36	0.21	0.23	0.48	0.54
0.1	0.3	0.04	0.04	0.22	0.26	0.13	0.16	0.39	0.42
0.1	0.7	0.00	0.00	0.08	0.08	0.04	0.04	0.19	0.17
0.3	0.01	0.11	0.10	0.43	0.46	0.33	0.34	0.46	0.54
0.3	0.05	0.10	0.08	0.34	0.31	0.27	0.25	0.39	0.39
0.3	0.1	0.08	0.07	0.25	0.24	0.21	0.20	0.36	0.32
0.3	0.2	0.04	0.04	0.17	0.16	0.14	0.13	0.24	0.24
0.3	0.3	0.03	0.03	0.11	0.12	0.08	0.09	0.19	0.18
0.3	0.7	0.00	0.00	0.04	0.04	0.03	0.02	0.10	0.07
0.6	0.01	0.06	0.07	0.19	0.25	0.17	0.21	0.23	0.29
0.6	0.1	0.03	0.05	0.15	0.13	0.12	0.12	0.17	0.17
0.6	0.2	0.03	0.03	0.10	0.09	0.09	0.08	0.14	0.12
0.6	0.3	0.02	0.02	0.07	0.06	0.06	0.05	0.12	0.10
0.9	0.05	0.05	0.05	0.10	0.11	0.09	0.11	0.13	0.14

Note:  $c_{B_1}$ —the concentration of ether,  
 $c_{B_2}$ —the concentration of dichloromethane,  
 $k'_e$ —experimental  $k'$ ,  
 $k'_c$ —calculated  $k'$ .

that are calculated from experimental data. The average deviations of experimental  $k'$  from the calculated  $k'$ ,  $\Delta = \frac{1}{N} \sum_{i=1}^N [(k'_e)_i - (k'_c)_i]$  are also listed in Table 2.

Table 2

The Constants in Eq. (28) and Average Deviations of Experimental  $k'$  From the Calculated  $k'$  for 11 Solutes

Solutes	Constants	$a$	$b_1$	$b_2$	$c_1$	$c_2$	$N$	$\Delta$
Fluoranthene		-2.38	-0.50	-3.55	-0.28	-0.074	35	0.0081
O-Nitrotoluene		-2.68	-0.34	-2.71	-0.50	-0.16	35	-0.0065
<i>p</i> -Nitrotoluene		-2.81	-0.42	-2.67	-0.55	-0.18	35	0.0025
O-Nitrochlorobenzene		-1.65	-0.76	-2.89	-0.32	-0.25	35	0.031
<i>p</i> -Nitrochlorobenzene		-2.97	-1.38	-2.23	-0.51	-0.18	35	0.025
Propyl Benzoate		-3.18	-0.64	-2.29	-0.80	-0.14	34	0.027
Methyl Phenyl Ketone		-1.61	-0.61	-2.11	-0.73	-0.11	30	0.10
Anthracene		-2.56	-0.21	-4.89	-0.35	0.015	35	-0.0043
Benzonitrile		-2.13	-0.65	-2.54	-0.61	-0.18	35	0.094
Nitrobenzene		-1.83	-0.69	-3.38	-0.40	-0.11	35	0.040
Benzyl Alcohol		-1.92	-0.54	-1.94	-0.65	-0.15	35	0.18

$$\text{Note: } \Delta = \frac{1}{N} \sum_{i=1}^N [(k'_e)_i - (k'_c)_i].$$

$N$ —The number of experimental datapoints.

### III. A FUNDAMENTAL RETENTION EQUATION FOR WEAK DISSOCIATIVE SOLUTE

Let solute  $H_2A$  be a weak acid, the dissociation equilibriums would exist in the mobile phase:



On the adsorbent surface, there are the equilibriums



The superscript "a" stands for the adsorption, "m" for the mobile phase, capital  $K$  represents equilibrium constant. When equilibriums between the mobile phase and adsorbent surface are established, we can write following expressions for Equilibriums (29) to (32)

$$K_1 = \frac{[HA^{-m}][H^+]}{[H_2A^m]}, \quad (34)$$

$$K_2 = \frac{[A^{-m}][H^+]}{[HA^{-m}]}, \quad (35)$$



$$K_3 = \frac{[\text{H}_2\text{A}^a]}{[\text{H}_2\text{A}^m]}, \quad (36)$$

$$K_4 = \frac{[\text{HA}^{-a}][\text{H}^+]}{[\text{H}_2\text{A}^a]}. \quad (37)$$

The mass distribution ratio  $\alpha$  of solute  $\text{H}_2\text{A}$  between the mobile phase and stationary phase is

$$\alpha = \frac{[\text{H}_2\text{A}^a] + [\text{HA}^{-a}]}{[\text{H}_2\text{A}^m] + [\text{HA}^{-m}] + [\text{A}^{-m}]}. \quad (38)$$

From the Eq. (34) to Eq. (37), we obtain

$$\alpha = K_3 \frac{1 + K_4/[\text{H}^+]}{1 + K_1/[\text{H}^+] + K_1K_2/[\text{H}^+]^2}, \quad (39)$$

where

$$K_4/[\text{H}^+] = [\text{HA}^{-a}]/[\text{H}_2\text{A}^a]. \quad (40)$$

For non-ion-exchangeable stationary phase, the adsorption of ion  $\text{HA}^-$  is much smaller than that of molecule  $\text{H}_2\text{A}$ , then  $K_4/[\text{H}^+] \ll 1$ , Eq. (39) can be written as

$$\alpha = K_3 \frac{1}{1 + K_1/[\text{H}^+] + K_1K_2/[\text{H}^+]^2}. \quad (41)$$

Therefore the logarithm of the capacity factor can be expressed as

$$\begin{aligned} \ln k'_{\text{acid}} &= \ln \left( \alpha \frac{V_s}{V_0} \right) = \ln \left( K_3 \frac{V_s}{V_0} \right) - \ln(1 + K_1/[\text{H}^+] + K_1K_2/[\text{H}^+]^2) \\ &= \ln k' - \ln(1 + K_1/[\text{H}^+] + K_1K_2/[\text{H}^+]^2), \end{aligned} \quad (42)$$

where  $V_s/V_0$  refers to the phase ratio. Substituting Eq. (27) into Eq. (42), the retention equation of weak acid can be obtained

$$\ln k'_{\text{acid}} = a + \sum_{i=1}^n b_i c_{B_i} + \sum_{i=1}^n c_i \ln c_{B_i} - \ln(1 + K_1/[\text{H}^+] + K_1K_2/[\text{H}^+]^2). \quad (43)$$

For monoacid,  $K_2$  is equal to zero, then,

$$\ln k'_{\text{acid}} = a + \sum_{i=1}^n b_i c_{B_i} + \sum_{i=1}^n c_i \ln c_{B_i} - \ln \left( 1 + \frac{K_1}{[\text{H}^+]} \right). \quad (44)$$

With similar method, the same expressions can be derived for a weak organic base and amphoteric compound, the results are as follows:

$$\begin{aligned} \ln k'_{\text{base}} &= a + \sum_{i=1}^n b_i c_{B_i} + \sum_{i=1}^n c_i \ln c_{B_i} - \ln(1 + 10^4 K_1 [\text{H}^+] \\ &\quad + 10^{28} K_1 K_2 [\text{H}^+]^2), \end{aligned} \quad (45)$$

$$\ln k'_{\text{am}} = a + \sum_{i=1}^n b_i c_{B_i} + \sum_{i=1}^n c_i \ln c_{B_i} - \ln \left( 1 + \frac{K_a}{[\text{H}^+]} + 10^4 K_b [\text{H}^+] \right). \quad (46)$$

The validity of Eq. (43) to Eq. (46) was proven by the experimental results<sup>[14]</sup>.

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