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## Superior reactivity of heterogeneous single-cluster catalysts for semihydrogenation of acetylene

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ABSTRACT Acetylene semi-hydrogenation is a vital process where the utilization of supported isolated Pd atoms as catalytic active sites is promising due to their unique reactivity and metal atom efficacy. In particular, doping Pd single atoms at different sites on metal-oxide surfaces provides an opportunity to regulate their local coordination environments and modulate their electronic and catalytic properties. In this study, we conduct extensive density functional theory calculations to investigate the influence of single Pd atom coordination environments and surface properties on the activity and selectivity of Pd<sub>1</sub>/TiO<sub>2</sub> catalysts for acetylene semihydrogenation. Considering the activity and selectivity, a fouratom single-cluster catalyst (SCC) of Pd<sub>1</sub>Ti<sub>3</sub>/TiO<sub>2</sub> with negatively charged  $Pd^{\delta-}$  sites is found to exhibit excellent catalytic performance. Moreover, both activity and selectivity are highly correlated with the surface properties, including the dband center index and surface work function. Our work provides theoretical guidance for the future design of heterogeneous SCC on reducible oxide supports for similar reactions in heterogeneous catalysis.

**Keywords:** acetylene, semi-hydrogenation, single-cluster catalysts (SCCs), TiO<sub>2</sub>, DFT

## INTRODUCTION

Semi-hydrogenation of acetylene in ethylene-rich streams is an industrially important process. This reaction is used to remove trace amounts of acetylene impurities in the feedstock for industrial ethylene polymerization to produce polyethylene [1]. The undesired acetylene content has to be removed from usually 0.1–1 vol% to lower than 5 ppm range, which would otherwise poison the downstream polymerization catalyst [2–4]. The hydrogenation catalysts are required to be effectively and selectively converting C–C triple bonds to double bonds, but not further to single ones. Therefore, how to understand the selectivity of semi-hydrogenation catalysts is scientifically attractive and designing new semi-hydrogenation catalysts with high selectivity is critical in industrial applications [5,6].

Palladium-based catalysts are commonly known for their excellent selectivity and widespread application in the semi-

hydrogenation of acetylene. Extensive research has been conducted to regulate the electronic and geometric structure of active clusters in order to suppress the over-hydrogenation of acetylene [6-9]. Among these efforts, the strategy of improving the isolation of active sites has garnered increasing interest to enhance the selectivity of hydrogenation products and achieve high metal atom efficacy. The forefront of this attempt is the development of single-atom catalysts (SACs) [10-13], which have been used successfully in hydrogenation reactions [14-22], oxidation reactions [10,23-29] and water-gas shift (WGS) reaction [30-33], etc. Zheng's group [15] provided a roomtemperature photochemical strategy to produce atomically dispersed Pd catalysts, and found that the Pd<sub>1</sub>/TiO<sub>2</sub> catalysts exhibit extremely high catalytic activity and stability in hydrogenation of C=C and C=O bonds. Lu's group [16] found that a Pd<sub>1</sub>/ graphene catalyst showed high selectivity of nearly 100% to butenes in the selective hydrogenation of 1,3-butadiene, with a conversion rate of 95%. Vilé et al. [20] carried out a joint experimental and theoretical study to propose that the high catalytic performance of the Pd<sub>1</sub>/C<sub>3</sub>N<sub>4</sub> system for the hydrogenation of alkynes was related to the favorable hydrogen activation and adsorption of alkynes on the atomically dispersed Pd sites. The intermetallic compounds with single-atom Pd sites achieved the high ethylene selectivity for semi-hydrogenation of acetylene [17,34,35].

Density functional theory (DFT) calculations demonstrated that the weak  $\pi$ -bonding for ethylene adsorption on the singleatom Pd sites suppresses its further hydrogenation, while the  $\sigma$ bonding for acetylene adsorption facilitates its hydrogenation. Some other single-atom alloy catalysts [36] also have high acetylene conversion and high selectivity to ethylene, such as Pd-Ag [36], Pd-Au [37] and Pt-Cu [38] alloys at the single-atom limit. Recently, the singly dispersed bimetallic Rh<sub>1</sub>Co<sub>3</sub> sites on CoO surface were identified to exhibit distinctly different catalytic performance in reduction of NO with CO and N2-to-NH3 thermal conversion [39-41]. The well-dispersed surfaceanchored metal clusters form a new type of catalysts named heterogeneous single-cluster catalyst (SCC) [42-49]. The graphdiyne-supported SCCs also have shown high selectivity for a series of reactions, including semi-hydrogenation of acetylene [43]. Therefore, the SCCs open up more opportunities to

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improve selectivity in hydrogenation reactions, and the atomiclevel understanding of this process is extremely important.

TiO<sub>2</sub> is commonly used as a support for the acetylene hydrogenation because of the role of reducible oxide support in the strong metal-support interaction phenomenon. The interaction between the oxide support and the metal particles is believed to have a significant impact on the catalyst activity and selectivity of the hydrogenation reaction [50,51]. Kim [52] found that TiO<sub>2</sub>-supported Pd catalysts have high ethylene selectivity for acetylene hydrogenation. Panpranot et al. [53] prepared Pd/ TiO<sub>2</sub> catalysts and clarified that the Ti<sup>3+</sup> in contact with Pd can probably reduce the adsorption strength of ethylene, thereby increasing the selectivity of ethylene. Yang et al. [54] investigated the reaction mechanism of selective hydrogenation of acetylene on Pd<sub>4</sub> clusters supported on anatase TiO<sub>2</sub> (101) and rutile TiO<sub>2</sub> (110), and found that the anatase TiO2 catalyst has higher selectivity of acetylene hydrogenation than the rutile one. Recently, Yang et al. [22] found that Pd<sub>1</sub>/TiO<sub>2</sub> has superior activity and selectivity in the selective semi-hydrogenation of phenylacetylene compared with commercial catalysts. In addition, it is also reported that Pd<sub>1</sub>/TiO<sub>2</sub> catalyst can facilitate the activation of O<sub>2</sub> into superoxide (O<sub>2</sub><sup>-</sup>) to promote the catalytic oxidation [55] and analyze the organophosphorus pesticide chlorpyrifos as a photocatalytic sensing platform [56], and so on.

Therefore, the utilization of  $TiO_2$ -supported isolated Pd atoms as catalytic active sites for acetylene semi-hydrogenation has garnered significant interest due to their distinct reactivity and efficient metal utilization. However, the relationship between the local coordination environment of Pd single atoms on the  $TiO_2$  surface and their catalytic activity and selectivity is yet to be understood. Thus, the main focus of this study is to elucidate the local structural and electronic properties of single Pd atoms located at different sites on the  $TiO_2$  (101) surface, as well as to investigate the reaction mechanism and catalytic behavior for semi-hydrogenation of acetylene on these  $Pd_1/TiO_2$  catalysts. The insights gained from these analyses can provide a theoretical foundation for the design of new SACs and SCCs for the semi-hydrogenation of acetylene.

## **EXPERIMENTAL SECTION**

All the calculations were carried out with Vienna ab initio simulation package (VASP) using spin-polarized DFT methods [57,58]. The projector augmented wave (PAW) method was chosen to describe the interactions between ions and valence electrons [59,60], and the exchange-correlation interaction of valence electrons was calculated by generalized gradient approximation in the Perdew-Burke-Ernzerhof form (GGA-PBE) [61]. The valence orbitals of Pd (4d, 5s), Ti (3d, 4s), O (2s, 2p), C (2s, 2p) and H (1s) were described by plane-wave basis sets with cutoff energies of 400 eV. The DFT + U approach was applied to the calculation of the electronic structure of TiO<sub>2</sub>, and the Hubbard parameters were set to U - J = 4 eV for Ti [62]. The Monkhorst-Pack  $(2 \times 2 \times 1)$  k-point grid sampling within Brillouin zones was used. The convergence criterium of the electronic self-consistent iteration was set to 10<sup>-4</sup> eV, and the residual force was set below 0.03 eV Å<sup>-1</sup>. The transition states (TSs) were searched using the improved dimer method [63] and the climbing image nudged elastic band (CI-NEB) method [64,65]. The electron density differences were evaluated using the formula  $\Delta \rho = \rho(Pd_1/substrate) - \rho(Pd_1) - \rho(substrate)$ . Atomic charges were computed using the atom-in-molecule (AIM) scheme proposed by Bader [66,67]. Crystal orbital Hamilton population (COHP) analysis was performed by using LOBSTER package [68,69].

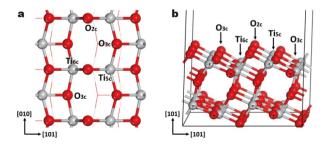
In this work, the calculated bulk lattice parameters of anatase  $TiO_2$  (a = 3.86 Å, c = 9.50 Å) are in agreement with the experimental data (a = 3.78 Å, c = 9.51 Å) [70]. For modeling  $TiO_2$  (101) surface, the  $p(2 \times 3)$  slab containing four layers of Ti atoms and eight layers of O atoms was used as shown in Fig. 1. In the calculations, the bottom five layers were fixed in their bulk position during geometry optimization. The vacuum layers were set to 15 Å for all supercells to avoid artificial interaction between the images. The adsorption energy of adsorbate was defined as  $E_{ads} = E(adsorbate/substrate) - E(substrate) +$ E(adsorbate), in which E(adsorbate/substrate), E(adsorbate), and E(substrate) are the calculated total energies of a substrate with the adsorbate, a gaseous-phase molecule (adsorbate), and a clean substrate, respectively. Based on the calculated harmonic vibrational frequencies, the zero-point vibration energies (ZPE) were evaluated and added in the electronic total energies.

#### **RESULTS AND DISCUSSION**

#### Surface model

It is well known that  $TiO_2$  (101) surface is the most stable and frequently exposed surface of anatase [71]. As shown in Fig. 1, the (101) surface presents a stepped structure, and has undercoordinated five-fold Ti ( $Ti_{5c}$ ) and two-fold O ( $O_{2c}$ ) atoms, as well as fully coordinated  $Ti_{6c}$  and two types of  $O_{3c}$  sites.

Experimentally, the precise synthesis of single atoms on the TiO<sub>2</sub> surface at different sites can be achieved through suitable preparation methods. For example, single atoms can be loaded onto the surface of a support material or doped at oxygen or metal defects [15,22,56,72-75]. Therefore, in order to explore the various potential configurations of a single Pd atom on the TiO<sub>2</sub> (101) surface, we have positioned the single-atom Pd at four different locations, as illustrated in Fig. 2. Fig. 2a, b show that the single-atom Pd substitutes an O<sub>2c</sub> and an O<sub>3c</sub> atom, respectively. In both cases, the anchored Pd atom is bonded to the Ti atoms, thus forming the Pd<sub>1</sub>Ti<sub>2</sub> and Pd<sub>1</sub>Ti<sub>3</sub> SCCs. The Pd atoms in both bimetallic positions obtain electrons from the lattice and form negatively charged Pd<sup>δ-</sup> ions (Table 1 and Fig. 2a, b). As presented in the projected density of state (PDOS, Fig. 3a, b), both 5s and 4d orbitals of Pd in Pd<sub>1</sub>Ti<sub>2</sub> and Pd<sub>1</sub>Ti<sub>3</sub> are found below Fermi level, respectively, indicating the formation of Pd $^{\delta-}$  anion. According to the binding energy, the Pd atom at Pd<sub>1</sub>Ti<sub>3</sub> site is slightly more stable than the Pd atom at Pd<sub>1</sub>Ti<sub>2</sub> site. Fig. 2c shows that the single-atom Pd substitutes a Ti<sub>5c</sub> atom (Pd<sub>Ti</sub> model), in which case the anchored Pd atom is bonded to five



**Figure 1** (a) Top and (b) side views of anatase  $TiO_2$  (101) supercell (O: red, Ti: gray).

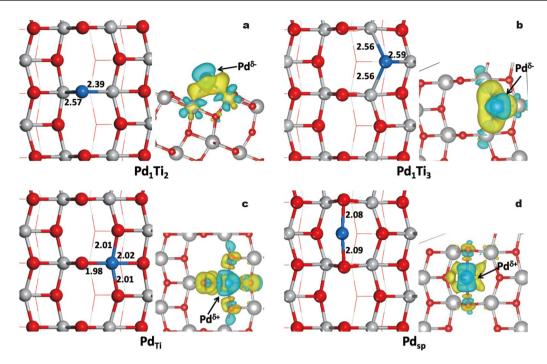
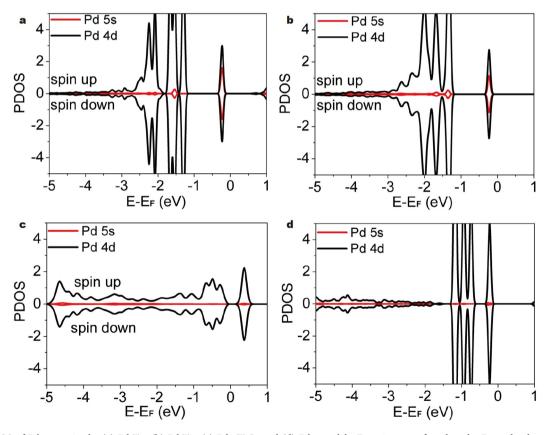


Figure 2 Optimized structures and calculated charge density differences for (a)  $Pd_1Ti_2$ , (b)  $Pd_1Ti_3$ , (c)  $Pd_{Ti}$  and (d)  $Pd_{sp}$  model configurations (O: red, Ti: gray, Pd: blue; the bond length in Å). Blue and yellow areas represent charge reduction and increase, respectively. The cutoff of the density-difference isosurfaces is equal to 0.004 electrons Å<sup>-3</sup>.

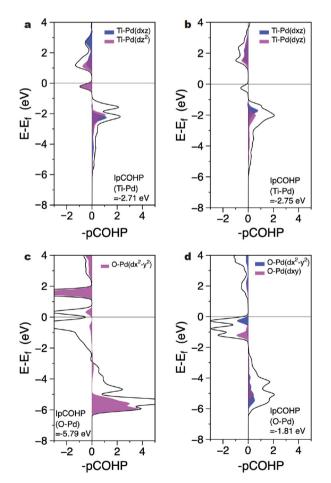


oxygen atoms with a positive charge of +1.52 |e| according to Bader charge analysis. The PDOS of Pd atom (Fig. 3c and Fig. S1) illustrates that the  $d_{x^2-y^2}$  orbital and a significant portion

of the  $d_{xz}$  orbital of the Pd single atom are unoccupied, while a portion of the  $d_{z^2}$  orbital is observed above the Fermi Level. This observation suggests that the oxidation state of the single-atom

Pd is approximately +4. The Pd atom in the  $Pd_{Ti}$  model is found to have the strongest binding energy among these four  $Pd_1/TiO_2$  models, indicating that the Pd substitution of  $Ti_{5c}$  on the  $TiO_2$  (101) surface is thermodynamically quite stable. Fig. 2d shows that the single-atom Pd is located on the surface ( $Pd_{sp}$  model). The Pd adatom prefers to locate at the bridge site between two  $O_{2c}$  atoms, which is consistent with previous work [76]. The calculated adsorption energy is -2.29 eV, and Pd-O bond lengths are 2.08 and 2.09 Å, respectively. The Bader charge analysis reveals that only 0.19 |e| are transferred from the metal to the oxide surface, leading to the formation of a slightly positively charged  $Pd^{\delta+}$  ion in this case. The PDOS in Fig. 3d shows that Pd adatom maintains the  $d^{10}$  electronic state because only 4d orbitals of Pd is found below Fermi level.

The COHP analysis was adopted to characterize the bonding orbitals and corresponding bonding strength. From the projected COHP analysis (Fig. 4), the Pd 4d and Ti 3d orbitals as well as Pd 4d and O 2p orbitals result in the bonding contributions below the Fermi level and most of the antibonding interactions above the Fermi level. For the Pd<sub>1</sub>Ti<sub>2</sub> model (Fig. 4a), the bonding contribution mainly comes from  $d_{xz}$  and  $d_{z^2}$  orbitals of Pd with the  $d_{xz}$  orbitals of two Ti atoms. For the Pd<sub>1</sub>Ti<sub>3</sub> model (Fig. 4b), the bonding is mainly caused by the  $d_{xz}$  and  $d_{yz}$  orbitals of Pd and the d orbitals of the three Ti atoms. As



**Figure 4** pCOHP between the metal center from Pd to Ti and O atoms on (a)  $Pd_1Ti_2$ , (b)  $Pd_1Ti_3$ , (c)  $Pd_{Ti}$  and (d)  $Pd_{sp}$  models and corresponding integrated values (IpCOHP). The negative value of -pCOHP represents the anti-bonding state, while the positive value of -pCOHP represents the bonding state.

presented in projected COHP (pCOHP) of  $Pd_{Ti}$  model (Fig. 4c), the splitting  $d_{x^2-y^2}$  of the Pd atom interacts with 2p orbital of five O atoms that stabilizes the binding of the Pd atom. As for the  $Pd_{sp}$  model (Fig. 4d), it is mainly the  $d_{xy}$  and  $d_{x^2-y^2}$  orbitals of the Pd atom and the 2p orbitals of the two O atoms that result in the bonding contribution. The integrated pCOHP (IpCOHP) can be used to quantify the bonding strength [77]. As presented in Fig. 4, the IpCOHP summed over all ligands of each Pd atom are -5.79, -2.75 and -2.71 eV in  $Pd_{Ti}$ ,  $Pd_1Ti_3$  and  $Pd_1Ti_2$  models, respectively. However, the IpCOHP of the Pd atom in  $Pd_{sp}$  model is only -1.81 eV, indicating that the bonding of the supported Pd atom is weaker than the bonding of the substituted Pd atom, which is consistent with the binding energy of single-atom Pd at different sites (Table 1).

## Adsorption properties of possible C<sub>2</sub>H<sub>x</sub> species on Pd<sub>1</sub>/TiO<sub>2</sub>

The adsorptions energies of C<sub>2</sub>H<sub>2</sub>, C<sub>2</sub>H<sub>3</sub>, C<sub>2</sub>H<sub>4</sub> and C<sub>2</sub>H<sub>5</sub> species on the four Pd<sub>1</sub>/TiO<sub>2</sub> models were firstly calculated to obtain the most stable configurations. The adsorption energies are presented in Fig. 5 and Table S1, the corresponding optimized structures are shown in Fig. S2. On these four Pd<sub>1</sub>/TiO<sub>2</sub> surfaces, the adsorption energies of acetylene and ethylene follow the order of  $Pd_1Ti_2 < Pd_{Ti} < Pd_1Ti_3 < Pd_{sp}$ . Both  $C_2H_2$  and  $C_2H_4$ favor the  $\pi$  adsorption mode in which two carbon atoms are bonded to the single-atom Pd. Due to the activation effect of Pd, the C-C bond length of the C<sub>2</sub>H<sub>x</sub> species on the Pd<sub>1</sub>/TiO<sub>2</sub> catalysts becomes longer than that of the gas-phase species. Among these four surfaces, Pd<sub>sp</sub> model has the greatest C<sub>2</sub>H<sub>4</sub> adsorption energy of -1.53 eV, indicating that ethylene is not conducive to desorption and may lead to the formation of undesired ethane. The most stable adsorption site for H is located on the O<sub>2c</sub> atom next to the Pd atom. The adsorption energy of H atoms shows a linear relationship with the Bader charge of the O atom on the different Pd<sub>1</sub>/TiO<sub>2</sub> models (Fig. S3). Specifically, the adsorption energy of H on Pd<sub>Ti</sub> (-2.14 eV) is significantly higher compared with the other three models. This is because in the Pd<sub>Ti</sub> model, the O atom connected to Pd has the least negative charge, making it more prone to electron uptake from H and thus exhibit the strongest H adsorption capability.

## C<sub>2</sub>H<sub>2</sub> hydrogenation mechanism

 $C_2H_2$  hydrogenation on  $Pd_1Ti_2$  model

The potential energy profile of  $C_2H_2$  hydrogenation on the  $Pd_1Ti_2$  model is shown by the black line in Fig. 6a, and the configurations of the TSs are shown in Fig. S4. The hydrogenation barriers ( $E_a$ ), reaction energies ( $E_r$ ) and the C–H distances at the TSs are summarized in Table S2. On the  $Pd_1Ti_2$  model,  $C_2H_2$  is adsorbed on the single-atom Pd with an

 Table 1
 Bader charges and binding energies of single-atom Pd at different sites<sup>a</sup>

	$Pd_1Ti_2$	$Pd_1Ti_3$	$Pd_{Ti}$	$Pd_{sp}$
Bader charge (Pd) ( e )	-0.74	-0.82	+1.52	+0.19
Binding energy (Pd) (eV)	-2.77	-3.20	-3.53	-2.29

a) The formation energy of Pd substituted surface (Pd<sub>Ti</sub>) was calculated using the equation: Pd(s) + Ti<sub>x</sub>O<sub>2x</sub>(surf) + O<sub>2</sub>(g)  $\rightarrow$  PdTi<sub>x-1</sub>O<sub>2x</sub>(surf) + TiO<sub>2</sub>(s).

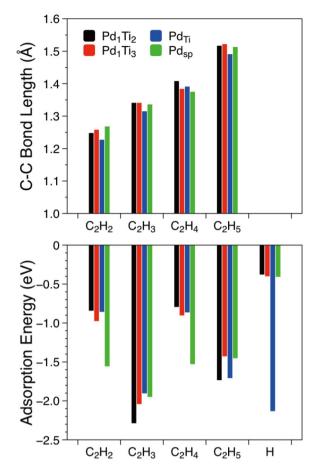


Figure 5 C–C bond lengths and adsorption energies of  $C_2H_x$  and H on  $Pd_1/TiO_2$  surfaces.

adsorption energy of -0.85 eV, which is conductive to hydrogenation to  $C_2H_4$  through the ethylene-like  $C_2H_3Pd$  intermediate (Fig. S2).  $C_2H_4$  also locates on the single Pd atom through a weak  $\pi$  bond, and the adsorption energy is -0.80 eV. It is found that the first hydrogenation step,  $C_2H_2^* + H^* \rightarrow C_2H_3^*$ , has the lowest activation barrier (0.44 eV) in the entire pathway and exothermic by 0.81 eV. The barriers of the next two steps are slightly higher, 1.19 eV for TS2 and 1.27 eV for TS3, and the reactions

are exothermic by 0.28 and 0.13 eV, respectively. The desorption energy of  $C_2H_4$  on  $Pd_1Ti_2$  model is 0.80 eV, smaller than its further hydrogenation barrier (1.27 eV). And the transition-state energy of  $C_2H_4$  hydrogenation (TS3) is higher than the energy of gas-phase ethylene (the black dotted line in Fig. 6a), which indicates that the ethylene is more prone to desorption in the subsequent process without further hydrogenation.

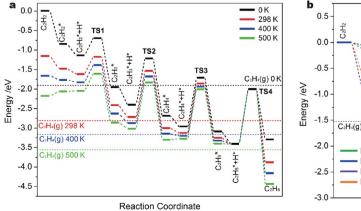
Since the temperature has a significant effect on the adsorption and desorption processes when entropy plays a significant role, we considered the entropic effects from gas phase acetylene and hydrogen to the gas phase ethane under standard pressure. The influence of the entropy is in the form of chemical potential, which can be obtained using the following equation:

$$\mu_{i}(T, p_{i}) = E_{i}(0 \text{ K}) + \widetilde{\mu}_{i}(T, p^{\theta}) + k_{B}T \ln \left(\frac{p_{i}}{p^{\theta}}\right).$$

 $E_i(0~{\rm K})$  is the DFT energy of the ideal gas molecule including zero-point energy;  $\widetilde{\mu}_i(T,p^\theta)$  includes the thermal contribution of ideal gas molecule and the entropy of ideal gas molecule at 1 atm (1 atm =  $1.01 \times 10^5$  Pa), which are given in the Supplementary information (Table S3). With the increase of temperature, the desorption of ethylene becomes much easier. At 400 K, the energy of adsorbed  $C_2H_4$  is higher than that of gasphase ethylene (the blue dashed line in Fig. 6a), suggesting the ethylene molecule desorbs from the surface spontaneously. Hence,  $Pd_1Ti_2$  SCC exhibits high selectivity in the semi-hydrogenation reaction of acetylene. When the temperature increases to 500 K (the green line in Fig. 6a), the adsorption of acetylene and hydrogen becomes unfavorable. Thus, entropic effects at 400 K are considered in the following discussion.

#### C<sub>2</sub>H<sub>2</sub> hydrogenation on Pd<sub>1</sub>Ti<sub>3</sub> model

The potential energy profile of acetylene hydrogenation on  $Pd_1Ti_3$  SCC at 400 K is shown as the blue line in Fig. 6b, and the configurations of the TSs are shown in Fig. S4. The barriers of  $C_2H_2$  and  $C_2H_3$  hydrogenation are 0.62 and 0.91 eV, and these two steps are highly exothermic by 0.67 and 1.00 eV, respectively (Table S2). The rate-limiting step of the entire process on  $Pd_1Ti_3$  SCC is the hydrogenation of  $C_2H_4$ , i.e.,  $C_2H_4^* + H^* \rightarrow C_2H_5^*$ , with a barrier of 1.33 eV and endothermicity of 0.42 eV. It is clear that the energy of  $C_2H_4^*$  is very close to the energy of gasphase ethylene at 400 K, and the hydrogenation barrier of  $C_2H_4$ 



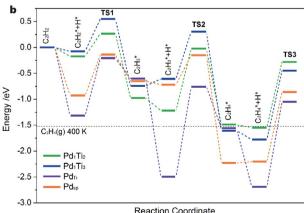


Figure 6 (a) Step-by-step hydrogenation mechanism of acetylene to ethane on the  $Pd_1Ti_2$  model at different temperatures. (b) Potential energy profiles of  $C_2H_2$  hydrogenation at 400 K on  $Pd_1/TiO_2$  surfaces.

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is much higher than its desorption energy, indicating that ethylene does not further hydrogenate, but desorbs from the surface. There, similar to  $Pd_1Ti_2$ ,  $Pd_1Ti_3$  SCC also has good selectivity in the semi-hydrogenation of  $C_2H_2$ .

## $C_2H_2$ hydrogenation on $Pd_{Ti}$ model

The potential energy profile for acetylene hydrogenation on Pd<sub>Ti</sub> model is shown as a purple line in Fig. 6b. As presented in Fig. 6b and Table S2, the hydrogenation of C<sub>2</sub>H<sub>2</sub> to C<sub>2</sub>H<sub>3</sub> has the lowest barrier in the entire hydrogenation process, with an activation energy of 1.10 eV (TS1) and endothermicity of 0.71 eV. The barrier of C<sub>2</sub>H<sub>3</sub> hydrogenation is 1.74 eV (TS2) and this step is endothermic by 0.94 eV. The energy of adsorbed C<sub>2</sub>H<sub>4</sub> is close to the energy of gas-phase C<sub>2</sub>H<sub>4</sub> at 400 K, which is much lower than its subsequent hydrogenation barrier (TS3, 1.64 eV), suggesting that the Pd<sub>Ti</sub> model will exhibit high selectivity in the semi-hydrogenation of C<sub>2</sub>H<sub>2</sub>. Since the H atom has a considerable adsorption energy (-2.14 eV) on the Pd atom of Pd<sub>Ti</sub> model, each hydrogenation step has a high barrier and is a strong endothermic process, which leads to a low activity of C<sub>2</sub>H<sub>2</sub> hydrogenation. The linear relationships between the hydrogen adsorption energies and C<sub>2</sub>H<sub>4</sub> formation energies as well as hydrogenation barriers of C<sub>2</sub>H<sub>4</sub> were found, as shown in Fig. S5.

## $C_2H_2$ hydrogenation on $Pd_{sp}$ model

The potential energy profile for  $C_2H_2$  hydrogenation on  $Pd_{sp}$  model is shown as an orange line in Fig. 6b. Among these four  $Pd_1/TiO_2$  models, the adsorption energy of  $C_2H_2$  and  $C_2H_4$  on

Pd<sub>sp</sub> model is the largest. The adsorption energy of  $C_2H_4$  is -1.53 eV, indicating that the desorption of  $C_2H_4$  is rather difficult. The barrier of the first hydrogenation step is 0.78 eV (TS1), and the reaction is slightly endothermic by 0.28 eV. The next step,  $C_2H_3^* + H^* \rightarrow C_2H_4^*$ , has a low barrier of 0.57 eV, and is highly exothermic by 1.51 eV, indicating that the Pd<sub>sp</sub> catalyst has high activity for  $C_2H_2$  hydrogenation. The further hydrogenation of  $C_2H_4$  to  $C_2H_5$  is the rate-determining step in the entire  $C_2H_2$  hydrogenation process, with a high barrier of 1.35 eV (TS3). However, the barrier (TS3) is still lower than the desorption energy of  $C_2H_4$ , and the energy of  $C_2H_4^*$  is much lower than the energy of gas-phase  $C_2H_4$  at 400 K. Thus,  $C_2H_4$  will be further hydrogenated before desorption from the surface, resulting in the formation of undesirable ethane.

## Ethylene selectivity on Pd<sub>1</sub>/TiO<sub>2</sub> surfaces

The selectivity between the semi-hydrogenation of  $C_2H_2$  to  $C_2H_4$  and the further hydrogenation to  $C_2H_6$  reaction depends on the adsorption energy of  $C_2H_4$  and the reaction barrier for its further hydrogenation (Fig. 7a). A lower adsorption energy of  $C_2H_4$  and a higher barrier for its further hydrogenation suggest that  $C_2H_4$  is more likely to desorb from the surface rather than undergo excessive hydrogenation. In this scenario, the catalyst demonstrates a higher selectivity towards  $C_2H_4$  formation. To quantitatively estimate the selectivity, we define  $\Delta E = E_a - |E_{ads}|$  as the difference between the hydrogenation barrier of  $C_2H_4$  ( $E_a$ ) and the absolute value of the adsorption energy of  $C_2H_4$  ( $E_a$ ) on these surfaces [78,79]. As indicated in Table S4, all catalysts, except for  $Pd_{sp}$ , exhibit positive  $\Delta E$  values. A positive  $\Delta E$  value

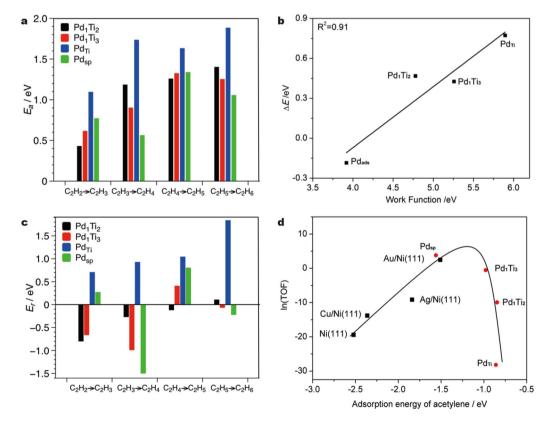


Figure 7 (a) Activation barriers for the hydrogenation of  $C_2H_2$  on  $Pd_1/TiO_2$  surfaces. (b) Relationship between  $\Delta E$  and work function of  $Pd_1/TiO_2$  surfaces. (c) Reaction energies for the hydrogenation of  $C_2H_2$  on  $Pd_1/TiO_2$  surfaces. (d) Volcano type of curve in which ln(TOF) is plotted as a function of the adsorption energies of  $C_2H_2$  (the black squares represent the data referenced from Ref. [78]).

signifies a preference for  $C_2H_4$  desorption over further hydrogenation, with larger  $\Delta E$  values corresponding to higher selectivity. Therefore, the selectivity of these four systems can be ranked as follows:  $Pd_{Ti} > Pd_1Ti_3 \approx Pd_1Ti_2 > Pd_{sp}$ . More importantly, a linear relationship is found between the  $\Delta E$  and surface work function (Fig. 7b). On the basis of these correlations, one can both predict the reactivity for  $C_2H_4$  formation on various surfaces via analyzing their surface properties and deduce the different dopants that can increase the  $C_2H_4$  selectivity in semi-hydrogenation of  $C_2H_2$ .

#### Activity of C<sub>2</sub>H<sub>2</sub> hydrogenation on Pd<sub>1</sub>/TiO<sub>2</sub> surfaces

In addition to selectivity, the different activities of acetylene hydrogenation on the four Pd<sub>1</sub>/TiO<sub>2</sub> models are also compared from both thermodynamic and kinetic perspectives. Thermodynamically, the reactivity of forming C<sub>2</sub>H<sub>4</sub> on the Pd<sub>1</sub>/TiO<sub>2</sub> surfaces can be described by the reaction energy of each hydrogenation step. As presented in Fig. 7c, each step of hydrogenation of C<sub>2</sub>H<sub>2</sub> on the Pd<sub>1</sub>Ti<sub>2</sub> model is an exothermic process. Similarly, in addition to the hydrogenation of C<sub>2</sub>H<sub>4</sub>, each hydrogenation step of C<sub>2</sub>H<sub>2</sub> on the Pd<sub>1</sub>Ti<sub>3</sub> model is exothermic. On the Pd<sub>sp</sub> model, the elementary step  $C_2H_3^* + H^* \rightarrow$ C<sub>2</sub>H<sub>4</sub>\* is the most exothermic reaction, while the hydrogenation of  $C_2H_2$  and  $C_2H_4$  is an endothermic process. The  $C_2H_2$ hydrogenation on the Pd<sub>Ti</sub> model is a thermodynamically unfavorable process, and each step is a strongly endothermic process. Furthermore, a linear relationship was found between the reaction energy of the entire reaction  $(C_2H_2^* + H_2 \rightarrow C_2H_4^*)$ and the d-band center index [80] of the single-atom Pd in the four systems (Fig. S6), indicating that the reaction energy increases with the increase of the d-band center of these Pd<sub>1</sub>/ TiO<sub>2</sub> surfaces. Among these four catalysts, C<sub>2</sub>H<sub>4</sub> formation on the Pd<sub>1</sub>Ti<sub>3</sub> SCC is the most thermodynamically favored, followed by Pd<sub>1</sub>Ti<sub>2</sub>, Pd<sub>sp</sub>, and Pd<sub>Ti</sub>.

Kinetically, the activity of the C2H2 hydrogenation can be estimated as following. According to the energetic span theory, the turnover frequencies (TOF) can be written  $ext{TOF} pprox rac{k_{ ext{B}}T}{h} \mathrm{e}^{-E_{ ext{a}}^{ ext{eff}}/RT},$  where  $E_{ ext{a}}^{ ext{eff}}$  is the effective barrier of the reaction, which is defined as the energy difference between the highest TS and the most stable intermediate species [78,81–83]. The estimated ln(TOF) was plotted against the adsorption energies of C<sub>2</sub>H<sub>2</sub> on the Pd<sub>1</sub>/TiO<sub>2</sub> surfaces as shown in Fig. 7d. Hu's group [78] investigated the activity of C<sub>2</sub>H<sub>4</sub> formation on Ni surfaces doped by Au, Ag, and Cu. They found the most inert dopant Au on the Ni surface weakens the C<sub>2</sub>H<sub>2</sub> adsorption and gives the highest activity. As can be seen from Fig. 7d, Pd<sub>sp</sub> and Ni catalysts are located on the strongly adsorbed side of the volcano curve, while Pd<sub>1</sub>Ti<sub>2</sub>, Pd<sub>1</sub>Ti<sub>3</sub>, and Pd<sub>Ti</sub> catalysts are located on the weakly adsorbed side. Among these systems, Pd<sub>sp</sub> and Pd<sub>1</sub>Ti<sub>3</sub> are the most active and very close to Au/Ni(111), followed by Pd<sub>1</sub>Ti<sub>2</sub>, while Pd<sub>Ti</sub> is the least active. The observed difference in activity can be attributed to the variation in the adsorption energy of H atoms on the different Pd<sub>1</sub>/TiO<sub>2</sub> models. In particular, the adsorption energy of H on Pd<sub>Ti</sub> is significantly higher compared with the other three models. Consequently, a higher energy barrier is required to activate the H atom from its initial adsorption state to the TS, resulting in a higher hydrogenation barrier on the Pd<sub>Ti</sub> model. Due to its low activity, the Pd<sub>Ti</sub> model is not considered a favorable candidate for C<sub>2</sub>H<sub>2</sub> semi-hydrogenation. Additionally, as previously discussed, Pd<sub>sp</sub> exhibits poor selectivity for  $C_2H_2$  semi-hydrogenation. Consequently, the  $Pd_1Ti_3$  SCC with bimetallic sites exhibits not only the highest selectivity but also the highest activity among the four  $Pd_1/TiO_2$  models when considering both thermodynamic and kinetic perspectives.

#### **CONCLUSIONS**

In this work, in order to reveal the underlying influence of single-atom Pd location and surface properties on the reaction performance, extensive DFT calculations are performed to elucidate the activity and selectivity of acetylene hydrogenation to ethylene on several Pd<sub>1</sub>/TiO<sub>2</sub> catalysts. The activity of different SACs Pd<sub>1</sub>/TiO<sub>2</sub> and SCCs for semi-hydrogenation of acetylene is found to follow the order of  $Pd_1Ti_3 \approx Pd_{sp} > Pd_1Ti_2 > Pd_{Ti}$ . The poor activity of Pd<sub>Ti</sub> model can be explained by the strong adsorption of the hydrogen atom on the surface. It is especially noteworthy that Pd<sub>1</sub>Ti<sub>3</sub> and Pd<sub>1</sub>Ti<sub>2</sub> SCCs have high selectivity for semi-hydrogenation of acetylene, while ethylene tends to be fully hydrogenated to ethane on Pd<sub>sp</sub> model. The Pd<sub>1</sub>Ti<sub>3</sub> SCC with negatively charged Pd<sup>δ-</sup> bimetallic sites exhibits excellent catalytic performance both in terms of activity and selectivity among all considered Pd<sub>1</sub>/TiO<sub>2</sub> catalysts. Moreover, both activity and selectivity are highly correlated with the surface properties, especially the d-band center index and surface work function. The catalyst with larger d-band center and surface work function has higher activity and selectivity. Our studies may provide a theoretical foundation for future design of highly efficient SCCs on reducible oxide supports for hydrogenation reactions in heterogeneous catalysis.

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**Author contributions** Li J supervised the project. Zhao S conceived the original concept, designed the experiments, and wrote the manuscript. Tang Y provided helpful discussion during the revision process. Yu X and Li J revised the manuscript, and all authors contributed to the general discussion.

**Conflict of interest** The authors declare that they have no conflict of interest.

**Supplementary information** Supporting data are available in the online version of the paper.



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**ARTICLES** 

## 单团簇催化剂在乙炔半加氢反应中的优异反应性

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摘要 载体上孤立的Pd原子作为乙炔半加氢反应的催化活性位点,由于具有独特的反应性和高效的金属利用率而备受关注.特别是在金属氧化物表面的不同位点掺杂Pd单原子,可以通过调节其局部配位环境来调控其电子和催化性能.本文采用密度泛函理论计算,研究了TiO2负载Pd单原子的局域配位环境对Pd<sub>1</sub>/TiO<sub>2</sub>催化剂上乙炔半加氢反应的活性和选择性的影响.综合考虑反应活性和选择性,发现具有负电荷Pd<sup>6</sup>位点的Pd<sub>1</sub>Ti<sub>3</sub>/TiO<sub>2</sub>四原子单团簇催化剂展现出优异的催化性能.此外,活性和选择性与表面性质如d-带中心指数和表面功函数等密切相关.本文为未来设计可还原氧化物载体上的高效单团簇催化剂以用于类似的多相催化反应提供了理论参考.