



利用微型可视毛细管反应器测定物质在高温高压水中溶解度

贝克，张传永，潘志彦*

浙江工业大学生物与环境工程学院，杭州 310032

* 联系人，E-mail: panzhiyan@zjut.edu.cn

2015-04-14 收稿, 2015-05-07 接受, 2015-05-19 网络版发表

国家自然科学基金(21377116, 21077092, 20777070)资助

摘要 目前无机盐和疏水性有机物在超/亚临界水中溶解度的研究虽已取得一定成果，但由于实验条件苛刻、设备要求高、操作难度大等问题，溶解度数据仍十分缺乏，无法满足现代工业应用要求，大大影响了超/亚临界流体技术在化学合成、萃取分离、环境工程等诸多领域的研究与开发进程，进一步确定高温高压水中物质的溶解度及其影响因素尚需要开展大量的基础研究工作。本文综述了无机盐和疏水性有机物在超/亚临界水中溶解度研究进展，并着重介绍了本课题组利用自行设计研发的耐高温高压微型可视毛细管反应器替代传统不锈钢材质高压反应釜或管式流反应器，结合显微放大观测技术、高精密冷热台、数字实时录像分析系统和拉曼光谱原位在线检测技术开展无机盐和疏水性有机物在超/亚临界水中溶解度研究工作取得的进展。

关键词

毛细管反应器
超/亚临界流体
溶解度
拉曼光谱

超/亚临界流体技术自20世纪70年代开始崭露头角，随后便以环保、绿色、高效等优点，被迅速应用到萃取分离、石油化工、化学反应工程、材料科学、生物技术、环境工程等诸多领域^[1~3]。常用的超/亚临界流体主要有H₂O, CO₂, CH₄等，其中水是自然界中存在最广泛的溶剂。研究表明，通过控制温度和压力可以改变超/亚临界水的极性、密度、扩散系数、表面张力和黏度等性质。处于高温高压状态的水具有介电常数小、扩散系数高、黏度低、密度低、能完全溶解有机物等特性^[4,5]。优良的溶解特性和反应特性，使超/亚临界水成为绿色化学领域关注研究的重点之一。

常温常压状态下，疏水性有机物一般被认为不溶或者微溶于水，其溶解度数据一直不为人们所重视。但是在高温高压条件下，随着介电常数的减小，超/亚临界水对疏水性有机物的溶解能力显著增强，

甚至可以达到完全互溶的状态。相比而言，无机盐在超/亚临界水中的溶解度却非常低，使得超/亚临界流体技术在实际应用过程中往往会遇到盐沉积引起的反应器内部管路堵塞等问题。同时，在高温高压及富氧条件下，盐类对反应器的腐蚀也较为严重^[6]。因此，掌握物质在超/亚临界水中的溶解度数据，构建准确的溶解模型，对超/亚临界水中化学反应动力学研究，对超/亚临界流体技术在化学合成、萃取分离、环境工程等领域的应用，以及高温高压反应器的设计、运行和优化均十分重要^[7]。

1 无机盐和疏水性有机物在超/亚临界水中溶解度研究进展

超/亚临界水中溶解度的测定从根本上说是高温高压状态下相平衡的研究。根据相平衡的确定方法，可以将无机盐和疏水性有机物在超/亚临界水中溶解

引用格式： 贝克，张传永，潘志彦. 利用微型可视毛细管反应器测定物质在高温高压水中溶解度. 科学通报, 2015, 60: 2500–2506

Bei K, Zhang C Y, Pan Z Y. Solubilities of inorganic salts and organic compounds in sub- and supercritical water in fused silica capillary reactor (in Chinese). Chin Sci Bull, 2015, 60: 2500–2506, doi: 10.1360/N972015-00301

度的测定方法分为2类：静态法和动态法(表S1).

1.1 静态法

静态法是将待测溶质和溶剂放置于固定体积的高压反应釜内，待足够长时间使体系达到平衡。静态法又可分为静态分析法和静态合成法^[8]。

静态分析法是将待测溶质和溶剂一起放置在密闭的高压釜中，待体系达到平衡后从高压釜中取样，并在常温常压下利用气相色谱、高效液相色谱等分析技术对取样进行分析，以获得相关溶解度数据。有学者使用上述实验方法和装置流程分别测定了苯、甲苯^[9]、乙醇+水+丙烯、异丙醇+水+丙烯三元体系^[10]、苯甲酸和水杨酸^[11]、萘普生^[12]、灰黄霉素^[13]、布地奈德^[14]、蒽^[15]、硬脂酸、软脂酸^[16]、羟苯甲酯、羟苯乙酯、羟苯丁酯^[17]等在超/亚临界水中的溶解度。

静态合成法是将预先配置好的已知浓度的物料放入高压釜中，逐渐改变体系的温度或压力，观察高压釜中样品的相态变化，当观察到某一相开始出现或消失，此时的温度、压力及已知的物料浓度即构成一个相边界点，以获得平衡条件下的溶解度数据。有学者使用上述实验方法和装置流程分别测定了K₂CO₃^[18]、Na₂SO₄^[19]、K₂SO₄^[20]、Li₂SO₄^[21]、Ge(OH)₄和GeO₂^[22]，苯、正庚烷、正戊烷、2-甲基戊烷、甲苯^[23]，苯酚^[24]等在超/亚临界水中的溶解度。

1.2 动态法

动态法是以一定的流速将一定浓度的高温高压溶液连续缓慢地通过高压釜，使水相和固相无机盐/油相疏水性有机物间在高压釜中建立平衡，然后对流出的溶液组分浓度进行分析。动态法又可分为多相法和单相法。

动态多相法是将预先混合好的溶液连续缓慢地通过高压釜，溶液在高压釜中停留足够长时间以达到相平衡，从取样口收集流出液进行组分分析。研究人员使用上述实验方法和装置流程分别测定了Na₂SO₄^[25~27]、Na₂CO₃^[27]、NaCl^[28,29]、KCl^[28]、MgCl₂、CaCl₂^[30]、Na₂HPO₄、NaH₂PO₄、MgSO₄^[31]，甲苯、葵烷^[32]，芘、蒽、苊、苊^[33]，对苯二甲酸^[34]等在超/亚临界水中的溶解度。

动态单相法是将固相无机盐/油相疏水性有机物置于高压釜中，使溶剂相连续缓慢地通过高压釜，与高压釜中溶质溶解饱和后流出，从取样口收集流出

液进行组分分析。研究人员使用上述实验方法和装置流程分别测定了萘^[35,36]、苯并[a]芘^[35]、苯、甲苯、间二甲苯、对异丙基甲苯、辛烷、三甲基戊烷、四氯乙烯、邻二氯苯、四乙基锡^[37]、蒽、苯并[a]蒽、苯并菲、三联苯^[36]、喹吖啶酮^[38]、木糖、葡萄糖、麦芽糖^[39]、无水槲皮素、二水槲皮素^[40]、没食子酸、儿茶酸、原儿茶酸^[41]等在超/亚临界水中的溶解度。

无机盐和疏水性有机物在超/亚临界水中溶解度的研究虽已取得一定成果，但由于高温高压实验条件苛刻、操作难度大、设备要求高，超/亚临界水中溶解度数据仍十分缺乏，无法满足现代工业应用要求。并且目前用于无机盐和疏水性有机物在超/亚临界水中溶解度测定的方法均存在一定的不足，传统用于超/亚临界水中溶解度测定的静态分析法取样过程容易破坏相平衡，静态合成法精确确定高压釜中样品的相变化点存在难度，动态法则难以保证取样分析时体系已达到相平衡。总体来说，进一步确定高温高压水中物质的溶解度及其影响因素尚需要开展大量的基础研究工作，并且仍缺乏一套安全环保、操作便捷，能精确测定高温高压流体溶解度的方法和装置。

2 微型可视毛细管反应器测定高温高压流体溶解度

本课题组利用自行设计研发的耐高温高压微型可视石英毛细管反应器(图1)替代传统不锈钢材质高压反应釜或管式流反应器，结合显微放大观测技术、高精密冷热台、数字实时录像分析系统和拉曼光谱原位在线检测技术开展无机盐和疏水性有机物在超/亚临界水中溶解度研究(图2)。此前，本课题组率先利用此类耐高温高压的微型可视石英毛细管反应器开展了超/亚临界水氧化氯苯^[42]、愈创木酚^[43]、超/亚临界水中四氯化碳^[44]、三氯乙烷^[45]水解，超/亚临界水及共溶剂中聚合物(聚碳酸酯^[46~49]、聚对苯



图 1 装有石英玻璃丝、水、疏水性有机物的密封毛细管反应器^[61](外径 665 μm，内径 300 μm，长度~1.5 cm)

Figure 1 An image of a sample in a fused silica capillary reactor (FSCR), showing hydrophobic organic compounds, water, vapour, and silica rod in the FSCR^[61] (0.3 mm I.D., 0.665 mm O.D., and ~1.5 cm long)

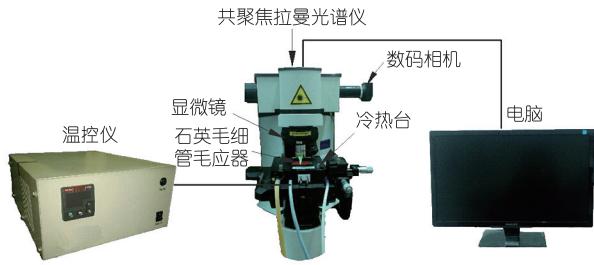


图2 冷热台-显微放大观测装置图。包括石英毛细管反应器、冷热台、数码相机、温控仪、显微镜、电脑和共聚焦拉曼光谱仪

Figure 2 Schematic diagram of the experimental apparatus including FSCR, heating-cooling stage, digital camera, temperature controller, microscope, computer, and confocal Raman spectrometer

二甲酸丁二醇酯^[50,51]、聚对苯二甲酸乙二醇酯^[52,53]、聚对苯二甲酸丙二醇酯^[54]、聚酰亚胺^[55,56]、聚对萘二甲酸乙二醇酯等解聚，亚临界水中聚合物单体(双酚A^[57]、对苯二甲酸等)的热稳定性，煤与塑料共液化^[58,59]、煤与聚苯乙烯共液化^[60]等研究，均取得了较为理想的结果。

将制备好的石英毛细管反应器放置于冷热台样品槽中，通过调节与冷热台相连的温度控制器精确控制体系温度，并将冷热台置于显微镜下。利用显微放大观测技术实时观测及记录无机盐和疏水性有机物在亚临界水中的相态变化，精确捕捉亚临界水体系中无机盐和疏水性有机物随温度升高过程中的晶体析出点和油-水界面消失点，以及温度降低过程中的晶体消失点和油-水界面重新出现点，同时结合拉曼光谱原位在线检测溶液体系的混合均匀度，确保溶液体系已达到相平衡，通过相界面的变化及拉曼谱带的积分强度测定无机盐和疏水性有机物在超/亚临界水中的溶解度^[61~63]。

为充分验证实验装置的可行性，课题组对目前亚临界水中溶解度研究较多的苯溶解度数据进行了测定。Chandler等人^[9]，Connolly^[23]，Miller和Hawthorne^[35]分别测定了苯在150~275℃，260~300℃和25~200℃水中的溶解度。本课题组^[62]实验测定了206.7~274.8℃苯的溶解度，实验数据具有良好的重现性，并且与文献报道值具有较好的吻合性(图3)。

在此基础上，本课题组^[61]首次采用显微原位在线放大观测-石英毛细管反应器(FSCR)实验测定装置，通过氯苯-水体系相界面随温度的变化，测定了氯苯在亚临界水中的溶解度(图4)，并对实验数据进行了拟合分析，得到173.3~266.9℃温度范围内氯苯

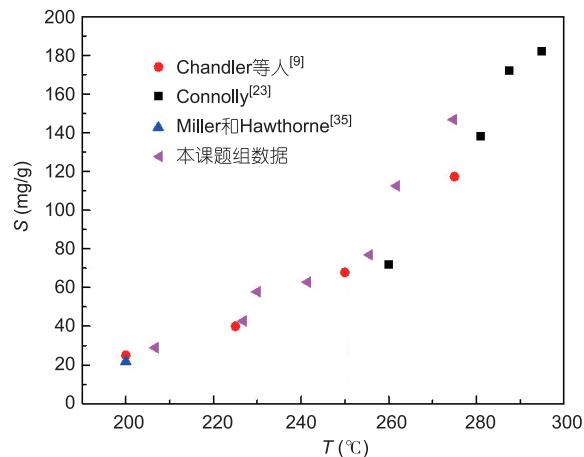


图3 苯在水中的溶解度数据与文献值的比较^[62]

Figure 3 The solubility of benzene from different sources^[62]

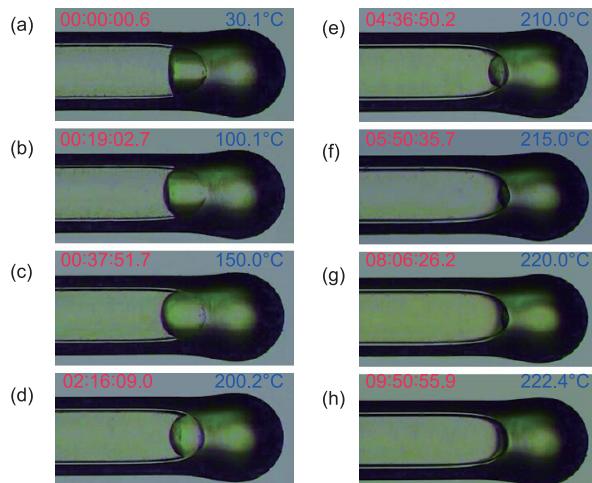


图4 氯苯在亚临界水中的溶解过程图^[61]。氯苯位于石英毛细管最右端，(a) 从室温30.1℃开始加热；(b)，(c) 氯苯先受热膨胀；(d)~(g)逐渐溶解；(h) 至222.4℃氯苯完全溶解

Figure 4 Dissolution of chlorobenzene in water during heating^[61]. The C_6H_5Cl is shown at the right end of the FSCR. (a) The images of C_6H_5Cl and H_2O in the capillary under the microscope at 30.1 °C. The C_6H_5Cl swelled between 100.0 and 150.0 °C (b), (c), dissolved between 200.2 and 220.0 °C (d)–(g) and dissolved totally at 222.4 °C (h)

在亚临界水中的溶解度数据，弥补了该温度区间氯苯溶解度数据的空缺。

此后，本课题组^[62]利用此类反应器对2,4-二氯甲苯在亚临界水中的溶解度进行了研究，初步探讨了疏水性有机物在亚临界水体系中的溶解规律，并利用石英毛细管显微装置结合拉曼光谱仪对苯-水体系和2,4-二氯甲苯-水体系升温过程及溶解平衡体系的均匀度进行了检验(图5)。

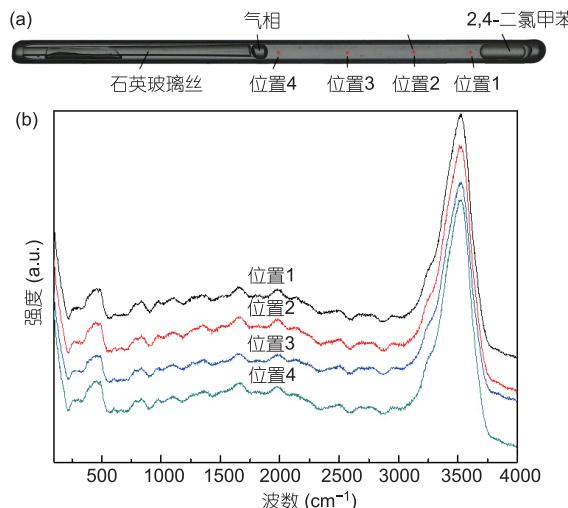


图 5 装有 2,4-二氯甲苯的石英毛细管反应器(a)及其拉曼光谱图(b)^[62]. (a) 2,4-二氯甲苯、均匀液相、气相、玻璃丝、拉曼光谱采集位置的样品图, 其中位置 1~4 为拉曼光谱的分析点位; (b) 220.0°C, 20 h 体系达到相平衡时在均匀液相采集的拉曼光谱图

Figure 5 Image of 2,4-dichlorotoluene in FSCR (a) and its Raman spectra (b)^[62]. (a) Showing 2,4-dichlorotoluene, liquid phase, vapor phase, and silica rod, and four spots for Raman analyses. (b) Raman spectra of liquid phase in the FSCR at 220.0°C, 20 h

此外, 本课题组^[63]还利用此类反应器开展了邻氯甲苯、对氯甲苯、2,4-二氯氟苯等疏水性有机物在亚临界水中溶解度、以及氯化钠、氯化钾、硫酸钙、硫酸镁、硫酸铜等无机盐在超/亚临界水中的溶解度和结晶介稳态研究。

3 总结

利用耐高温高压微型可视石英毛细管反应器开展无机盐和疏水性有机物溶解度研究, 该方法将样品容器体积缩小至微升级, 具有低耗、直观、安全等优良性能, 而且不需取样分析, 直接可以进行观测记录, 并可结合拉曼光谱进行原位在线检测分析, 为无机盐和疏水性有机物在高温高压水中溶解性能的研究提供了一种新的方法。

目前, 本课题组正逐步将该类反应器的应用领域由固-液、液-液体系扩展到气(超临界流体)-液体系的溶解度研究, 相继开展了CO₂在乙醇中溶解度及CO₂盐水层中溶解度研究。

参考文献

- Ikushima Y, Hatakeyama K, Sato O, et al. Noncatalytic organic synthesis using supercritical water: The peculiarity near the critical point. *Angew Chem Int Ed*, 1999, 38: 2910–2914
- Tollbäck J, Bigatá M B, Crescenzi C, et al. Feasibility of analyzing fine particulate matter in air using solid-phase extraction membranes and dynamic subcritical water extraction. *Anal Chem*, 2008, 80: 3159–3167
- Kamali H, Ghaziaskar H S. Pressurized hot water extraction of benzoic acid and phthalic anhydride from petrochemical wastes using a modified supercritical fluid extractor and a central composite design for optimization. *J Supercrit Fluids*, 2010, 54: 16–21
- Dinjus E, Kruse A. Hot compressed water—A suitable and sustainable solvent and reaction medium? *J Phys Condens Matter*, 2004, 16: S1161–S1169
- Kruse A, Dinjus E. Hot compressed water as reaction medium and reactant: Properties and synthesis reactions. *J Supercrit Fluids*, 2007, 39: 362–380
- Ma C Y, Jiang A X, Peng Y L, et al. Corrosion of titanic alloy steels in chlorine wastewater solution by supercritical water oxidation (in Chinese). *J Yunnan Univ Nat Sci Ed*, 2006, 28: 274–276 [马承愚, 姜安玺, 彭英利, 等. 钛合金在超临界水氧化含氯废水介质中腐蚀的研究. 云南大学学报(自然科学版), 2006, 28: 274–276]
- Fredenslund A, Jones R L, Prausnitz J M. Group-contribution estimation of activity coefficients in nonideal liquid mixtures. *AIChE J*, 1975, 21: 1086–1099
- Galia A, Argentino A, Scialdone O, et al. A new simple static method for the determination of solubilities of condensed compounds in supercritical fluids. *J Supercrit Fluids*, 2002, 24: 7–17
- Chandler K, Eason B, Liotta C L, et al. Phase equilibria for binary aqueous systems from a near-critical water reaction apparatus. *Ind Eng Chem Res*, 1998, 37: 3515–3518
- Rojas A, Gros H P, Mabe G, et al. Liquid-liquid equilibrium for the ethanol + water + propylene and 2-propanol + water + propylene systems from subcritical to near-critical conditions. *J Chem Eng Data*, 1999, 44: 693–695
- Kayan B, Yang Y, Lindquist E J, et al. Solubility of benzoic and salicylic acids in subcritical water at temperatures ranging from 298 to 473 K. *J Chem Eng Data*, 2010, 55: 2229–2232

- 12 Carr A G, Mammucari R, Foster N R. Solubility, solubility modeling, and precipitation of naproxen from subcritical water solutions. *Ind Eng Chem Res*, 2010, 49: 9385–9393
- 13 Carr A G, Mammucari R, Foster N R. Solubility and micronization of griseofulvin in subcritical water. *Ind Eng Chem Res*, 2010, 49: 3403–3410
- 14 Carr A G, Branch A, Mammucari R, et al. The solubility and solubility modelling of budesonide in pure and modified subcritical water solutions. *J Supercrit Fluids*, 2010, 55: 37–42
- 15 Teoh W H, Mammucari R, Vieira de Melo S A B, et al. Solubility and solubility modeling of polycyclic aromatic hydrocarbons in subcritical water. *Ind Eng Chem Res*, 2013, 52: 5806–5814
- 16 Huang P, Yang R, Qiu T, et al. Solubility of fatty acids in subcritical water. *J Supercrit Fluids*, 2013, 81: 221–225
- 17 Kapalavavi B, Ankney J, Baucom M, et al. Solubility of parabens in subcritical water. *J Chem Eng Data*, 2014, 59: 912–916
- 18 Moore R C, Mesmer R E, Simonson J M. Solubility of potassium carbonate in water between 384 and 529 K measured using the synthetic method. *J Chem Eng Data*, 1997, 42: 1078–1081
- 19 Hurst W S, Hodes M S, Bowers W J, et al. Optical flow cell and apparatus for solubility, salt deposition and Raman spectroscopic studies in aqueous solutions near the water critical point. *J Supercrit Fluids*, 2002, 22: 157–166
- 20 Hodes M, Griffith P, Smith K A, et al. Salt solubility and deposition in high temperature and pressure aqueous solutions. *AIChE J*, 2004, 50: 2038–2049
- 21 Abdulagatov I M, Azizov N D. Experimental vapor pressures and derived thermodynamic properties of aqueous solutions of lithium sulfate from 423 to 573 K. *Fluid Phase Equilib*, 2004, 216: 189–199
- 22 Pokrovski G S, Roux J, Hazemann J L, et al. An X-ray absorption spectroscopy study of argutite solubility and aqueous Ge(IV) speciation in hydrothermal fluids to 500°C and 400 bar. *Chem Geol*, 2005, 217: 127–145
- 23 Connolly J F. Solubility of hydrocarbons in water near the critical solution temperatures. *J Chem Eng Data*, 1966, 11: 13–16
- 24 Ni L, Wang X B, Zhang L, et al. Study on critical solution temperature of water-phenol by means of cloud point (in Chinese). *J Jiangsu Univ Nat Sci Ed*, 2006, 27: 364–367 [倪良, 王学宝, 张莉, 等. 浊点法研究水-苯酚系统的临界溶解温度. 江苏大学学报(自然科学版), 2006, 27: 364–367]
- 25 Shvedov D, Tremaine P R. The solubility of sodium sulfate and the reduction of aqueous sulfate by magnetite under near-critical conditions. *J Solut Chem*, 2000, 29: 889–904
- 26 Xiang B T, Wang T, Chen Z. The solubility of sodium sulfate in supercritical water (in Chinese). *Chem Eng*, 2001, 29: 72–74 [向波涛, 王涛, 陈璐. 超临界水中硫酸钠溶解度研究. 化学工程, 2001, 29: 72–74]
- 27 Khan M S, Rogak S N. Solubility of Na₂SO₄, Na₂CO₃ and their mixture in supercritical water. *J Supercrit Fluids*, 2004, 30: 359–373
- 28 Higashi H, Iwai Y, Matsumoto K, et al. Measurement and correlation for solubilities of alkali metal chlorides in water vapor at high temperature and pressure. *Fluid Phase Equilib*, 2005, 228: 547–551
- 29 Leusbrock I, Metz S J, Rexwinkel G, et al. Quantitative approaches for the description of solubilities of inorganic compounds in near-critical and supercritical water. *J Supercrit Fluids*, 2008, 47: 117–127
- 30 Leusbrock I, Metz S J, Rexwinkel G, et al. The solubility of magnesium chloride and calcium chloride in near-critical and supercritical water. *J Supercrit Fluids*, 2010, 53: 17–24
- 31 Leusbrock I, Metz S J, Rexwinkel G, et al. The solubilities of phosphate and sulfate salts in supercritical water. *J Supercrit Fluids*, 2010, 54: 1–8
- 32 Haruki M, Iwai Y, Nagao S, et al. Measurement and correlation of phase equilibria for water+ hydrocarbon systems near the critical temperature and pressure of water. *Ind Eng Chem Res*, 2000, 39: 4516–4520
- 33 Andersson T A, Hartonen K M, Riekkola M L. Solubility of acenaphthene, anthracene, and pyrene in water at 50°C to 300°C. *J Chem Eng Data*, 2005, 50: 1177–1183
- 34 Takebayashi Y, Sue K, Yoda S, et al. Solubility of terephthalic acid in subcritical water. *J Chem Eng Data*, 2012, 57: 1810–1816
- 35 Miller D J, Hawthorne S B. Method for determining the solubilities of hydrophobic organics in subcritical water. *Anal Chem*, 1998, 70: 1618–1621
- 36 Karásek P, Planeta J, Roth M. Solubility of solid polycyclic aromatic hydrocarbons in pressurized hot water at temperatures from 313 K to the melting point. *J Chem Eng Data*, 2006, 51: 616–622
- 37 Miller D J, Hawthorne S B. Solubility of liquid organics of environmental interest in subcritical (hot/liquid) water from 298 K to 473 K. *J Chem Eng Data*, 2000, 45: 78–81
- 38 Sue K, Usami T, Arai K, et al. Quinacridone solubility in hot-compressed water. *J Chem Eng Data*, 2007, 52: 714–717
- 39 Zhang D, Montanés F, Srinivas K, et al. Measurement and correlation of the solubility of carbohydrates in subcritical water. *Ind Eng Chem Res*, 2010, 49: 6691–6698

- 40 Srinivas K, King J W, Howard L R, et al. Solubility and solution thermodynamic properties of quercetin and quercetin dihydrate in subcritical water. *J Food Eng*, 2010, 100: 208–218
- 41 Srinivas K, King J W, Howard L R, et al. Solubility of gallic acid, catechin, and protocatechuic acid in subcritical water from 298.75 to 415.85 K. *J Chem Eng Data*, 2010, 55: 3101–3108
- 42 Liu H C, Pan Z Y. Visual observations and Raman spectroscopic studies of supercritical water oxidation of chlorobenzene in an anticorrosive fused-silica capillary reactor. *Environ Sci Technol*, 2012, 46: 3384–3389
- 43 Jin J J, Wang J L, Shen Y, et al. Visual and Raman spectroscopic observations of hot compressed water oxidation of guaiacol in fused silica capillary reactors. *J Supercrit Fluids*, 2014, 95: 546–552
- 44 Chen Y J, Jin Z F, Pan Z Y. *In situ* Raman spectroscopic study of hydrolysis of carbon tetrachloride in hot compressed water in a fused silica capillary reactor. *J Supercrit Fluids*, 2012, 72: 22–27
- 45 He W J, Jin Z F, Wang J L, et al. Decomposition of 1,1,1-trichloroethane in hot compressed water in anti-corrosive fused silica capillary reactor and Raman spectroscopic measurement of CO₂ product. *Chem Eng Sci*, 2013, 94: 185–191
- 46 Pan Z Y, Chou I M, Burruss R C. Hydrolysis of polycarbonate in sub-critical water in fused silica capillary reactor with *in situ* Raman spectroscopy. *Green Chem*, 2009, 11: 1105–1107
- 47 Huang Y Y, Liu S X, Pan Z Y. Effects of plastic additives on depolymerization of polycarbonate in sub-critical water. *Polym Degrad Stab*, 2011, 96: 1405–1410
- 48 Liu S X, Pan Z Y, Zou X, et al. Depolymerization of polycarbonate in sub-critical water (in Chinese). *Acta Polym Sin*, 2011, (3): 254–260 [柳世袭, 潘志彦, 邹霞, 等. 聚碳酸酯在亚临界水中解聚的研究. 高分子学报, 2011, (3): 254–260]
- 49 Pan Z Y, Hu Z C, Shi Y H, et al. Depolymerization of polycarbonate with catalyst in hot compressed water in fused silica capillary and autoclave reactors. *RSC Adv*, 2014, 4: 19992–19998
- 50 Liu L, Dai J J, Huang Y Y, et al. Catalytic depolymerization of polybutylene terephthalate in subcritical water (in Chinese). *J Chem Eng Chin Univ*, 2012, 26: 524–530 [刘丽, 戴娟娟, 黄园园, 等. 聚对苯二甲酸丁二醇酯在亚临界水中的催化解聚. 高校化学工程学报, 2012, 26: 524–530]
- 51 Pan Z Y, Shi Y H, Liu L, et al. Depolymerization of poly (butylene terephthalate) in sub- and supercritical ethanol in a fused silica capillary reactor or autoclave reactor. *Polym Degrad Stab*, 2013, 98: 1287–1292
- 52 Wang M X, Pan Z Y, Dai J J, et al. Depolymerization of polyethylene terephthalate in sub- and supercritical water (in Chinese). *J Chem Eng Chin Univ*, 2011, 25: 904–910 [王媚娟, 潘志彦, 戴娟娟, 等. 超/亚临界水中聚对苯二甲酸乙二醇酯的解聚. 高校化学工程学报, 2011, 25: 904–910]
- 53 Liu Y P, Wang M X, Pan Z Y. Catalytic depolymerization of polyethylene terephthalate in hot compressed water. *J Supercrit Fluids*, 2012, 62: 226–231
- 54 Gao J, Jin Z F, Pan Z Y. Depolymerization of poly (trimethylene terephthalate) in hot compressed water at 240–320°C. *Polym Degrad Stab*, 2012, 97: 1838–1843
- 55 Huang Y Y, Jin Z F, Liu L, et al. The depolymerization of polyimide and the stability of 4,4-diaminodiphenyl ether in sub-critical water (in Chinese). *Acta Sci Circumst*, 2011, 31: 2154–2161 [黄园园, 金赞芳, 刘丽, 等. 亚临界水中聚酰亚胺的解聚及其单体稳定性的研究. 环境科学学报, 2011, 31: 2154–2161]
- 56 Huang F, Huang Y Y, Pan Z Y. Depolymerization of ODPA/ODA polyimide in a fused silica capillary reactor and batch autoclave reactor from 320 to 350°C in hot compressed water. *Ind Eng Chem Res*, 2012, 51: 7001–7006
- 57 Liu Y P, Jin Z F, Liu L, et al. Stability of bisphenol A in high-temperature water in fused silica capillary reactor (in Chinese). *CIESC J*, 2011, 62: 2527–2534 [柳颖萍, 金赞芳, 刘丽, 等. 石英毛细管反应器内双酚 A 在高温水中的稳定性. 化工学报, 2011, 62: 2527–2534]
- 58 Shen Y, Wu H Y, Pan Z Y. Co-liquefaction of coal and polypropylene or polystyrene in hot compressed water at 360–430°C. *Fuel Process Technol*, 2012, 104: 281–286
- 59 Shen Y, Wu H Y, Li Y, et al. Coliquefaction of coal and polystyrene in supercritical water. *Int J Green Energy*, 2015, doi: 10.1080/15435075.2014.961463
- 60 Wu H Y, Pan Z Y, Jin Z F, et al. Co-liquefaction of coal and polystyrene in supercritical water (in Chinese). *J Fuel Chem Technol*, 2011, 39: 246–250 [吴海燕, 潘志彦, 金赞芳, 等. 超临界水中煤与聚苯乙烯的共液化研究. 燃料化学学报, 2011, 39: 246–250]
- 61 Pan Z Y, Dong Z. Determination of chlorobenzene solubilities in subcritical water in a fused silica capillary reactor from 173 to 267°C. *Ind Eng Chem Res*, 2011, 50: 11724–11727
- 62 Pan Z Y, Ma Y P, Chou I M. Solubility of 2,4-dichlorotoluene in water determined in fused silica capillary reactor by *in situ* Raman spectroscopy. *AIChE J*, 2013, 59: 2721–2725

- 63 Zhou L, Pan Z Y, Lin C M, et al. Advances in study on solubility of inorganic salts in supercritical water (in Chinese). Mod Chem Ind, 2010, 30: 33–37 [周黎, 潘志彦, 林春绵, 等. 无机盐在超临界水中溶解性研究进展. 现代化工, 2010, 30: 33–37]

Solubilities of inorganic salts and organic compounds in sub- and supercritical water in fused silica capillary reactor

BEI Ke, ZHANG ChuanYong & PAN ZhiYan

College of Biological & Environmental Engineering, Zhejiang University of Technology, Hangzhou 310032, China

Some meaningful achievements have been made on the solubilities of inorganic salts and organic compounds in sub- and supercritical water. But the solubility data remain too scarce to meet the need of modern industry due to the harsh of experimental conditions, equipment requirements and experimental operations, which greatly affects the research and development processes of sub- and supercritical fluid technology in chemical synthesis, extraction and separation, environmental engineering and many other fields. Basic researches still need to be carried out to determine the solubility data and its influence factors of substances in sub- and supercritical water. This paper reviews the research advances of inorganic salts and organic compounds solubility in sub- and supercritical water. The developments of the solubilities of inorganic salts and organic compounds in sub- and supercritical water in fused silica capillary reactor, instead of the traditional stainless steel autoclave or tubular flow reactor, combined with microscopic observation, heating-cooling stage, real-time digital video and *in-situ* Raman designed by author's group are highlighted in this paper.

fused silica capillary reactor, sub- and supercritical water, solubility, Raman spectroscopy

doi: 10.1360/N972015-00301

补充材料

表 S1 无机盐和疏水性有机物在超/亚临界水中溶解度测定方法汇总

本文以上补充材料见网络版 csb.scichina.com. 补充材料为作者提供的原始数据, 作者对其学术质量和内容负责.